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# Fuel Effects on NOx Control

2006 NOx Round Table

Kevin Davis & Connie Senior •  Reaction Engineering Int'l

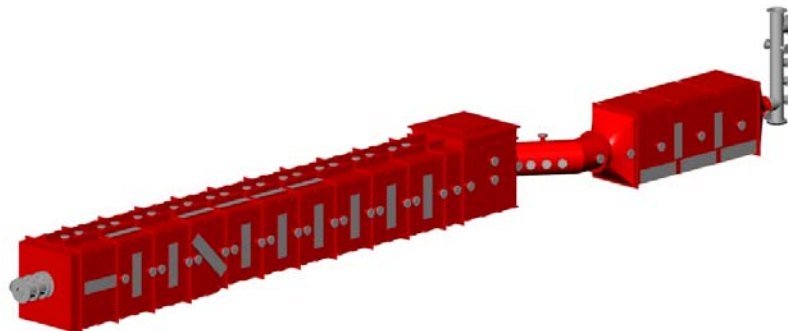
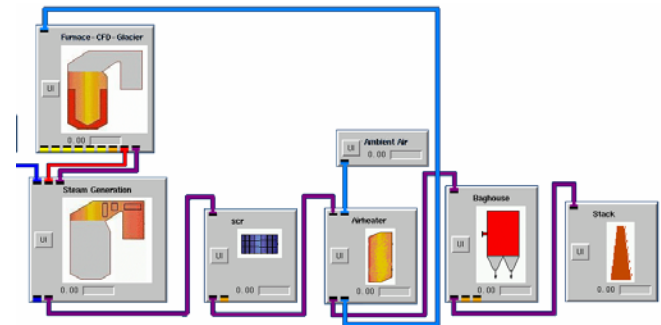
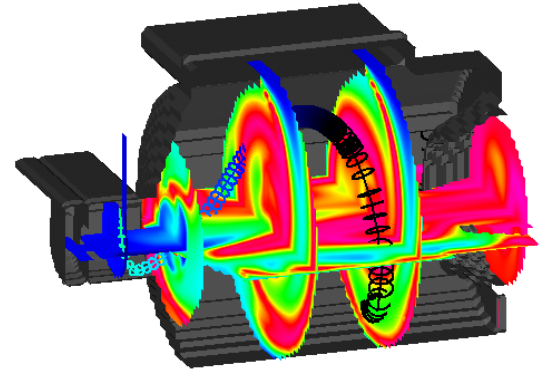
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# Introduction to REI

- ➔ Simulations for Utility/Industrial Applications  
Performance, emissions, operational impacts
- ➔ Customized Software  
Simplified unit-specific CFD tools, advanced process simulation software, chemical kinetic software
- ➔ Specialized Equipment  
Development and evaluation of equipment and instrumentation concepts
- ➔ Proof-of-Concept Testing  
Access to a unique collection of lab and pilot-scale facilities at the University of Utah



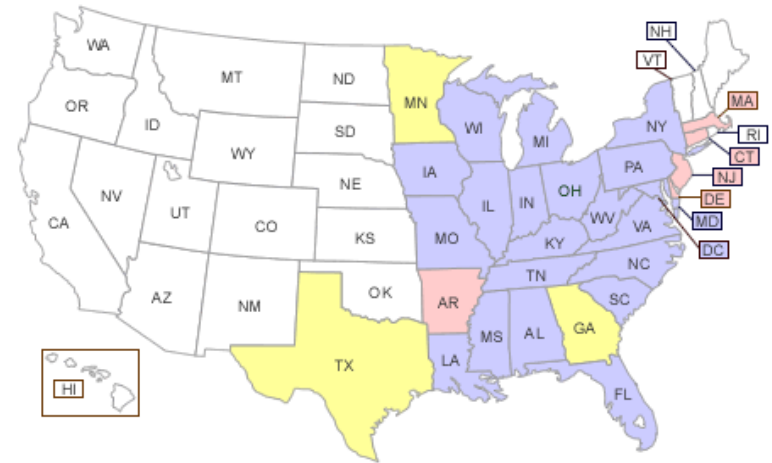
# Recent Utility NO<sub>x</sub> Regulations

## → CAIR

- ◆ permanent, year-round cap in 28 states and DC
- ◆ implemented through SIPs
- ◆ 0.15 lbs/MMBtu by 2010 and 0.125 lbs/MMBtu by 2015

## → Regional Haze

- ◆ new driver for non-CAIR (western) plants in regions near 156 national parks/wilderness areas
- ◆ implemented through SIPs, due on or before end of 2008
- ◆ BART compliance within five years of SIP



■ ozone and particles  
■ ozone only  
■ particles only  
■ not covered by CAIR

# Fuel Selection Issues

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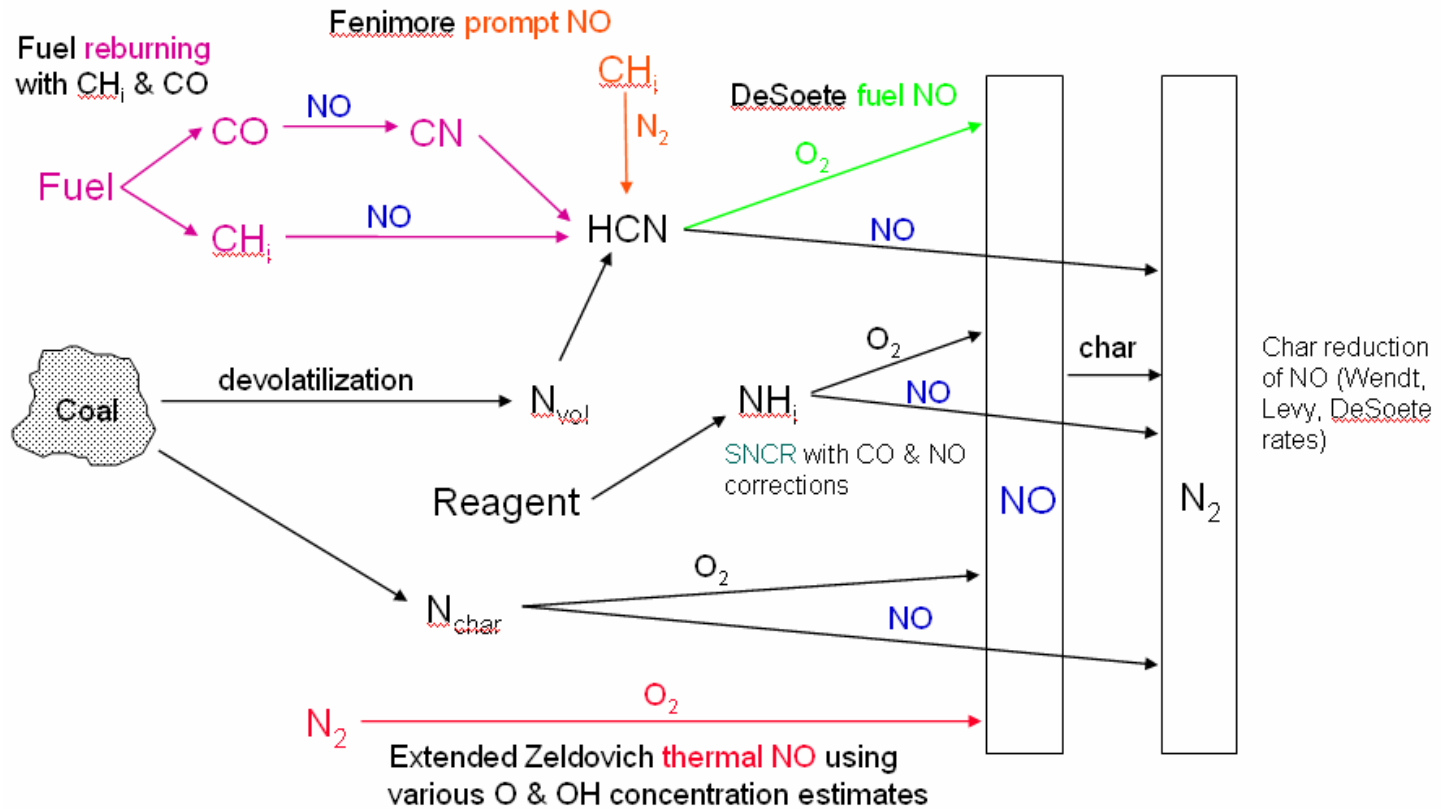
- ➔ **Regulatory pressures**
- ➔ **Equipment compatibility**
- ➔ **Asian demand for low sulfur compliance coals**
- ➔ **Mine/seam or transportation availability**
- ➔ **Emphasis on renewable fuels**



- ➔ Coal – anthracite, bituminous coal, subbituminous coal, lignite, blends
- ➔ Opportunity fuels – petcoke, woodwaste, agricultural residues, TDF, RDF
- ➔ Specialty fuels – synfuel, micronized coal

# NOx Fundamentals

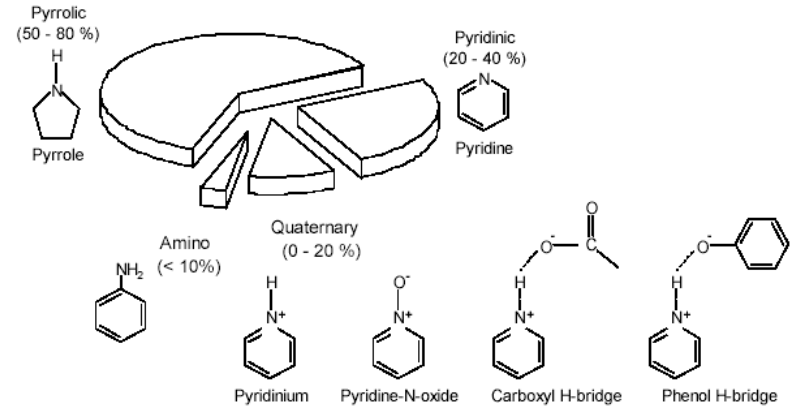
- ➔ Fuel NOx
- ➔ Thermal NOx
- ➔ Prompt NOx



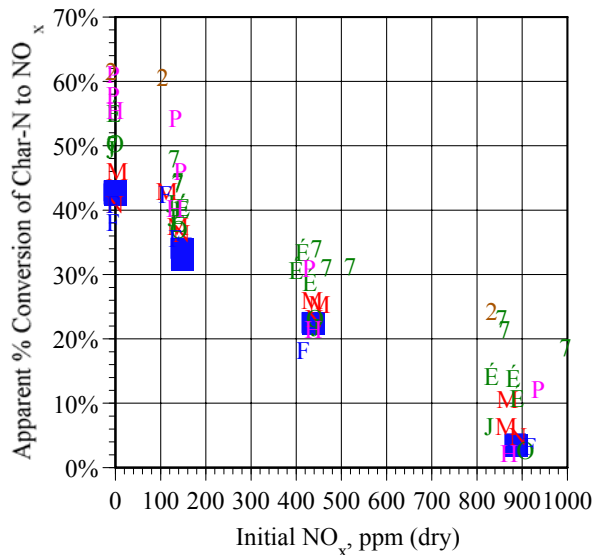
# Fuel NO<sub>x</sub>

## → Fuel NO<sub>x</sub> from pyrolysis

- ◆ Fuel nitrogen content
- ◆ Pyrolysis yield (coal rank)
- ◆ Preferential nitrogen release



Molina, PhD Thesis (2002)



- Pitt (25,26,29 sept)-1.0 wt%N
- N Pitt (19,24 oct)-1.06 wt%N
- M Pitt (27,28,29 sept)-1.14 wt%N
- J Ill (14,19,20,21 sept)-1.13 wt%N
- O Ill (16 oct)-1.13 wt%N
- É Ill (22 sept)-1.28 wt%N
- 7 Ill (18 sept)-1.61 wt%N
- F Utah (13 sept)-1.14 wt%N
- H K.R. (26 oct)-0.46 wt%N
- P K.R. (31 oct,1 nov)-0.51 wt%N
- 2 Black Thunder-0.48 wt%N

## → Fuel NO<sub>x</sub> from char oxidation

- ◆ Char yield
- ◆ NO<sub>x</sub> in gas-phase

# In-furnace NOx Control Technologies

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- Air Staging (low NOx burners, over-fire air, biasing)
- Fuel Switching and additives (nitrogen content, volatility, preferential nitrogen release)
- Fuel Staging (reburn, lower fire incremental respacing)
- Amine Injection (SNCR, Rich Reagent Injection)
- Tempering (flue gas recirculation, water/steam injection, air preheat reduction)
- Combustion Control/Optimization
  - ♦ monitoring of coal flow, air flow, emissions, flame stability, carbon-in-flyash, corrosion
  - ♦ simple or advanced control schemes
- Oxygen (targeted injection, nitrogen elimination & CO<sub>2</sub> recycle)
- Technology Hybrids and Layering
- Multi-pollutant Developments

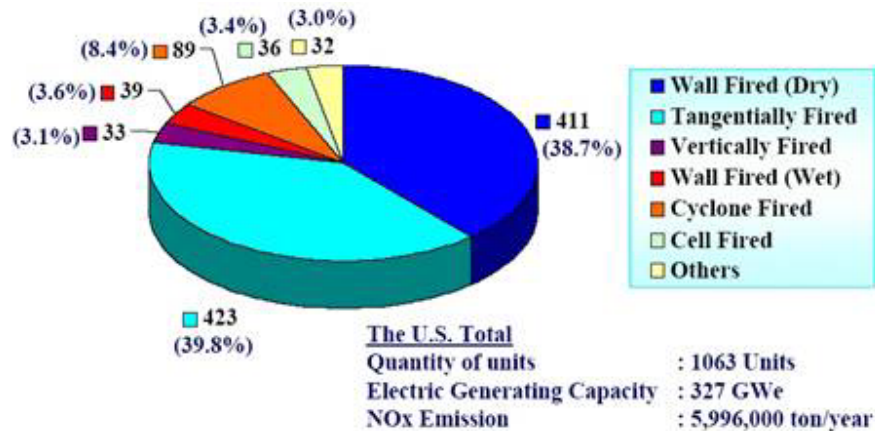
# Low-NO<sub>x</sub> Burners and Over-fire Air

Boiler Type <sup>a</sup>	Coal Type	Primary Control Technology	1995 Average Baseline NO <sub>x</sub> Emission (lb/10 <sup>6</sup> Btu)	2003 Average Controlled NO <sub>x</sub> Emission (lb/10 <sup>6</sup> Btu)	Average NO <sub>x</sub> Reduction Efficiency (%)	Range of NO <sub>x</sub> Reduction Efficiencies (%)	No. of Boilers
Wall-fired	Bituminous	LNB	0.71	0.41	39.2	8.6–70.1	62
Wall-fired	Bituminous	LNBO	0.81	0.35	53.3	32.7–71.9	16
Wall-fired	Subbituminous	LNB	0.59	0.28	45.5	19.4–80.3	16
Wall-fired	Subbituminous	LNBO	0.41	0.14	63.4	40.0–80.9	4
Tangential-fired	Bituminous	LNC1	0.62	0.39	35.0	17.2–65.4	26
Tangential-fired	Bituminous	LNC2	0.48	0.31	36.6	23.3–70.8	15
Tangential-fired	Bituminous	LNC3	0.56	0.25	54.9	38.1–72.2	19
Tangential-fired	Subbituminous	LNC1	0.38	0.21	45.4	11.3–74.4	18
Tangential-fired	Subbituminous	LNC2	0.43	0.23	45.6	33.9–65.4	3
Tangential-fired	Subbituminous	LNC3	0.35	0.14	60.5	48.2–77.2	23

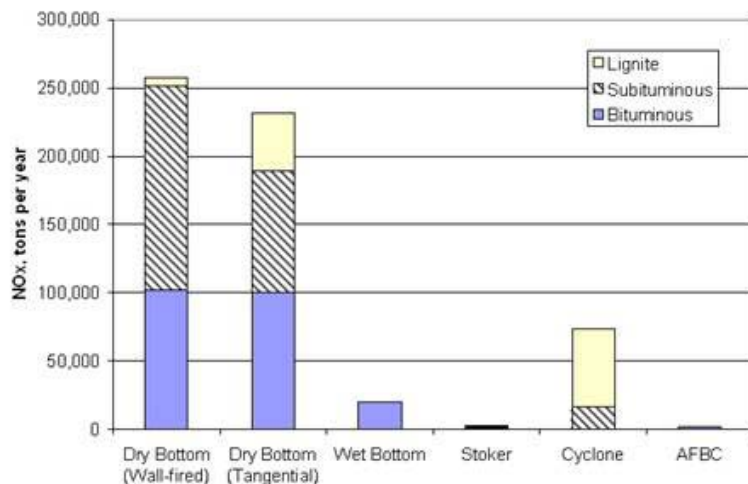
Notes: LNB = low-NO<sub>x</sub> burner; LNBO = LNB with OFA; LNC1 = LNB with close-coupled OFA; LNC2 = LNB with separated OFA; and LNC3 = LNB with both close-coupled and separated OFA. <sup>a</sup>All boilers are dry-bottom type.

Srivastava et al., JAWMA (2005)

# Firing Configurations and NOx Emissions



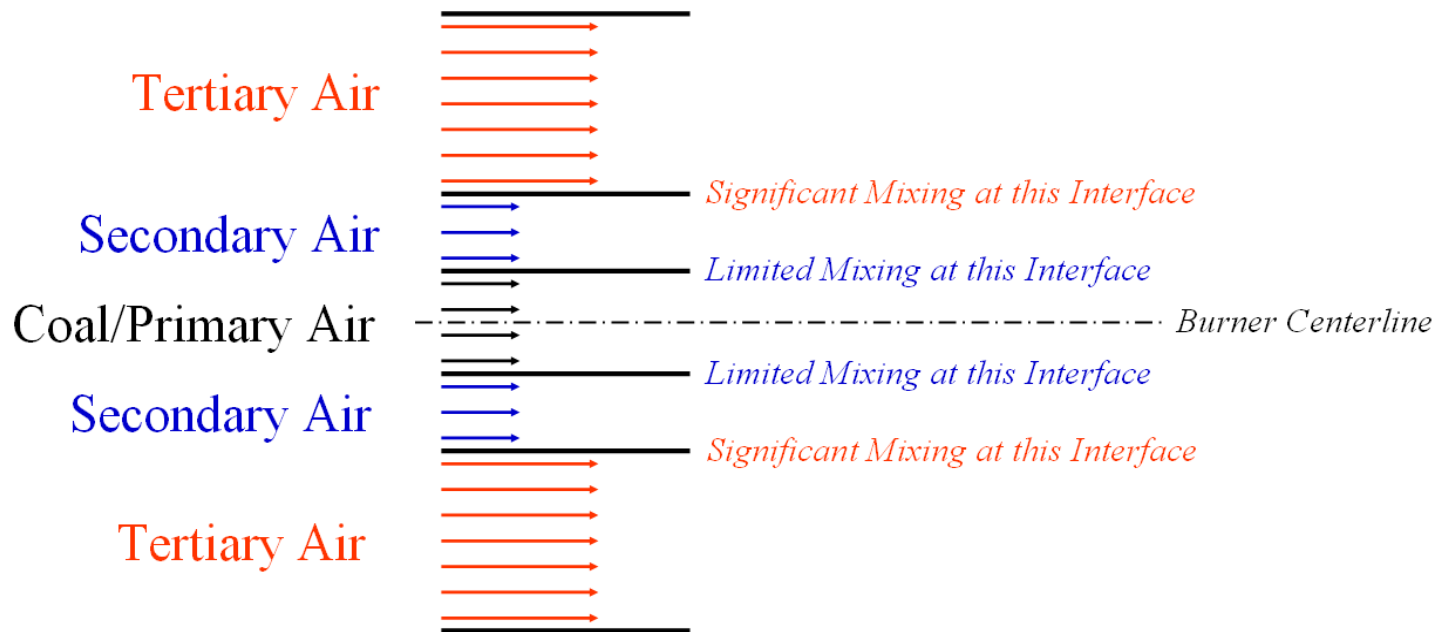
Source : DOE Fossil Energy – Low NOx Clean Technology Burners (1990)



WRAP, 1996

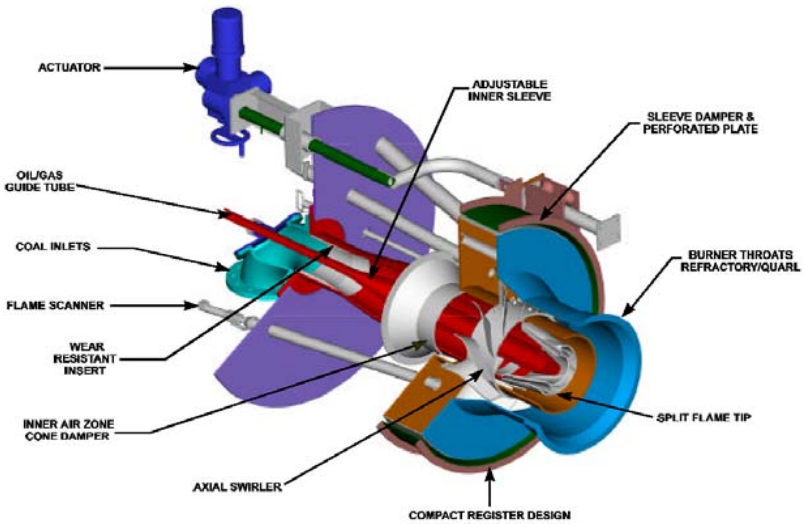
- ➔ Wall- and corner-fired units dominate US coal-fired generation
- ➔ Cyclone-fired units are also important due to their relatively high NOx production
- ➔ Control technology selection can be firing system dependent

# Early Low NOx Burner Approach

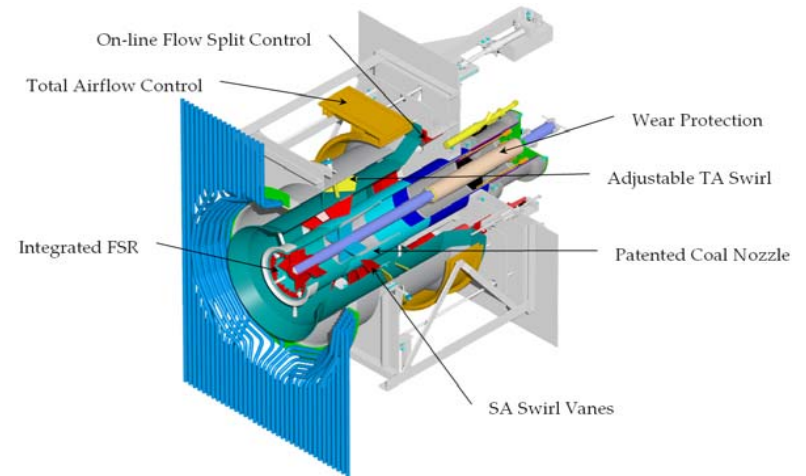


- ➔ **Minimize fuel transport air**
- ➔ **Secondary air stream delays mixing of air with fuel**
- ➔ **Peak flame temperatures and available oxygen in the flame can be reduced**
- ➔ **Practice and theory often at odds due to equipment limitations and simplistic view**

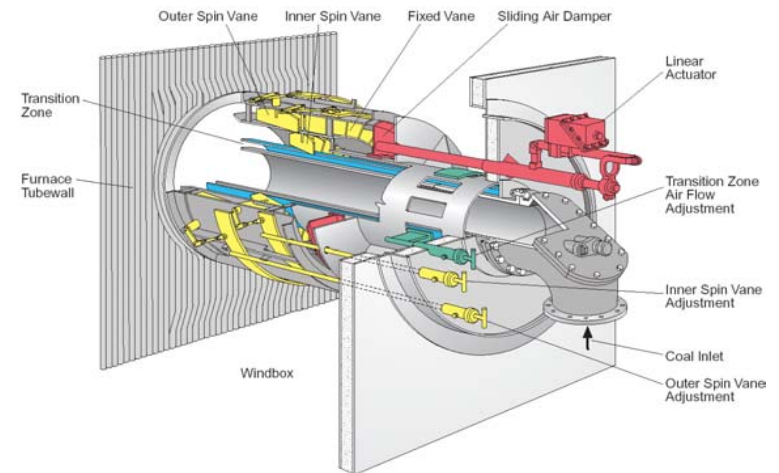
# Advanced Low NOx Swirl Burners



Foster Wheeler Vortex



Babcock & Wilcox DRB-4Z



Riley Power CCV-DAZ

# LNB Performance and Developments

Low-NO<sub>x</sub> Burner Retrofit Performance and Costs

Boiler Type	Wall-Fired	T-Fired	Cell Burner
Technology	LNB	LNCFS I	LNCB
Size, MWe	500	200	600
NO <sub>x</sub> Reduction, %	48	37	55
Capital Cost, \$/kW	6	7	9

DOE Clean Coal Technology Topical Report (1996)

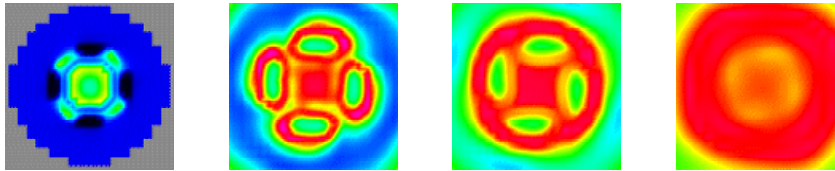
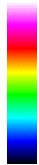


Takahashi (2001)

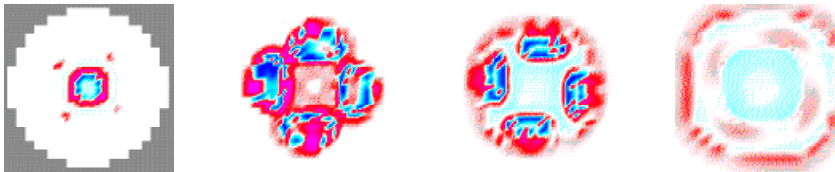
- Fuel concentration in primary air stream to create NO<sub>x</sub> reducing regions and improve flame stability
  - ◆ Reductions in primary air to fuel ratio using improved mills and ducting
  - ◆ Creation of local enrichment in particle loading (coal spreaders, Foster Wheeler Split Flame, Riley Venturi, B&W diffuser)
  
- Physical and aerodynamic creation of recirculation zones in/near fuel rich regions
  - ◆ Burner core bluff bodies or low velocity flows
  - ◆ Hitachi coal pipe ring
  - ◆ Riley Power secondary air diverter
  
- Independent control of secondary and tertiary swirl and flow

# NOx Formation and Reduction in LNBs

Temperature



NOx Rate



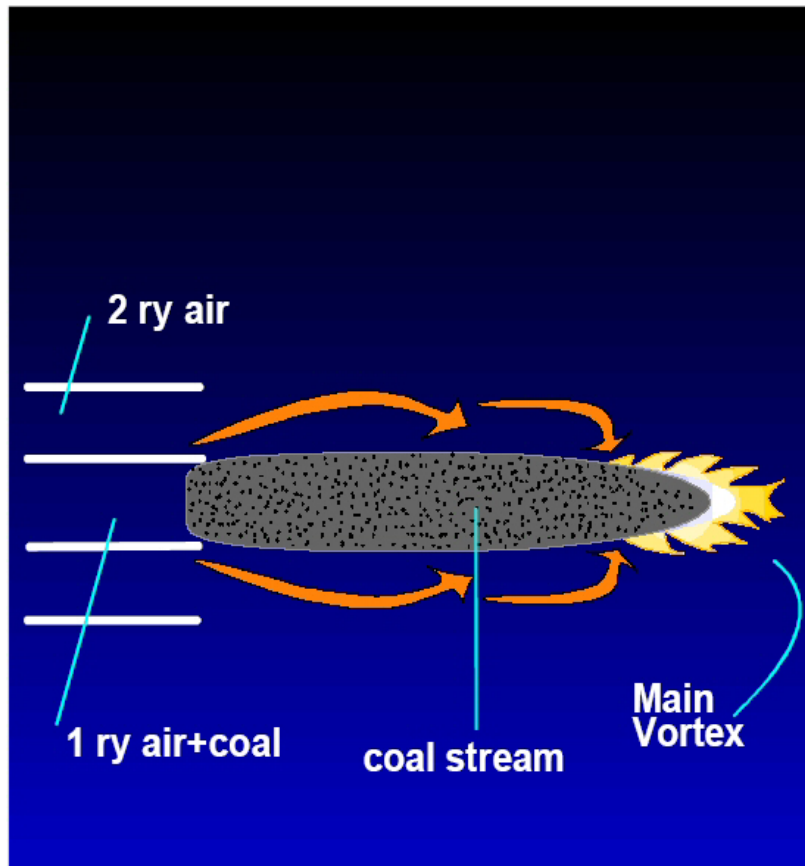
→ Increasing distance from burner face →



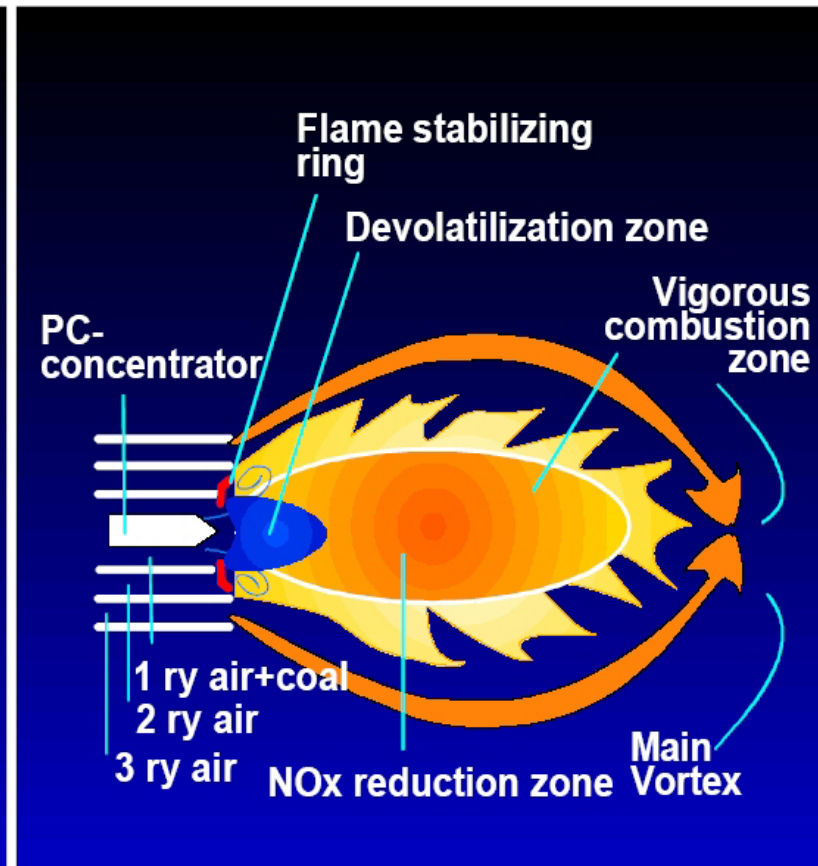
Courtesy of Southern Company

# Hitachi High Swirl Approach

Conventional JET burner



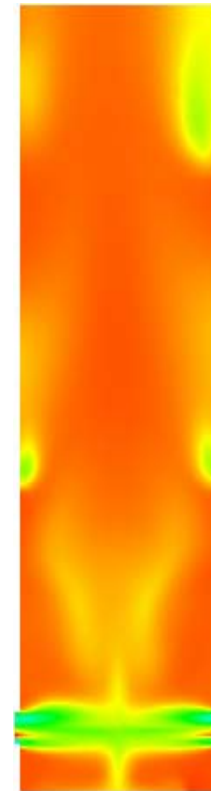
Improved burner



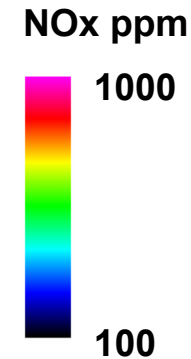
Takahashi (2001)

# Overfire Air

- Fuel rich chemistry reduces formation of NO<sub>x</sub> and, given adequate reaction time, can destroy a portion of the NO<sub>x</sub> formed initially
- Final addition of air is staged significantly, allowing heat to be removed prior to completion of oxidation

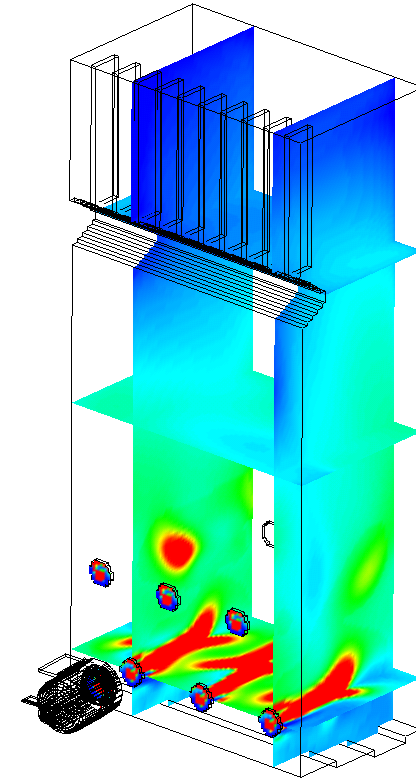
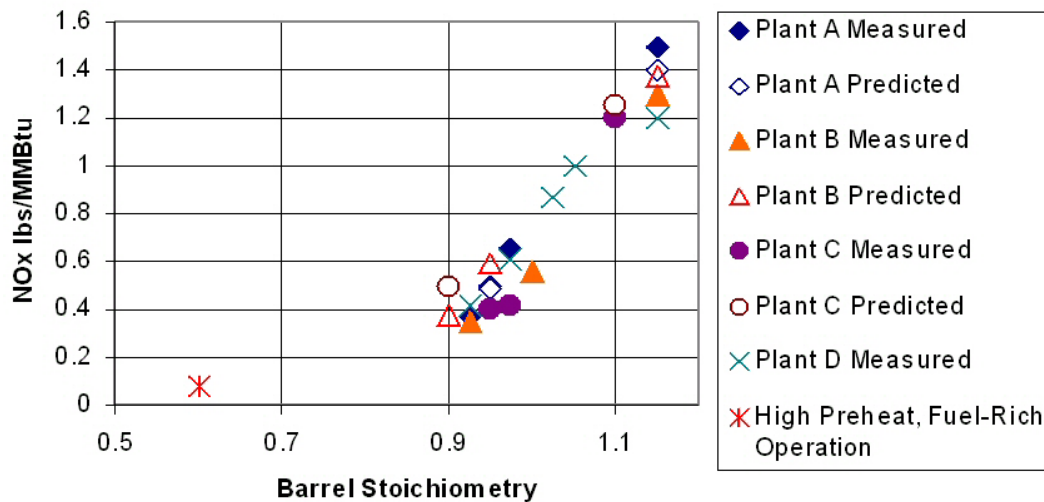


Baseline

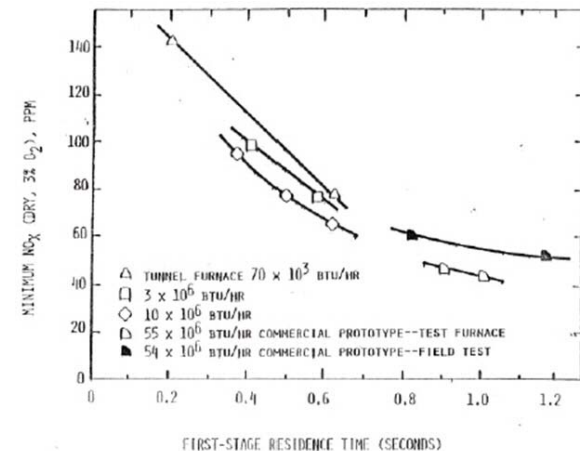


Staged

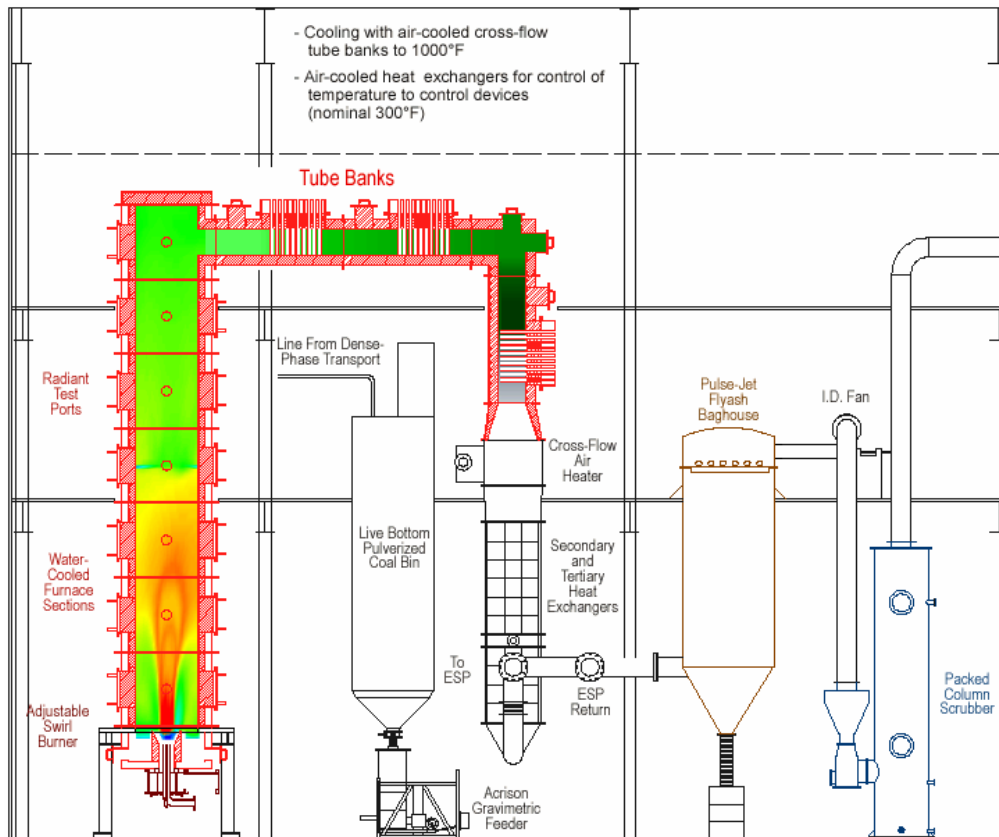
# Air Staging Stoichiometry



- ➔ Staging reaches an optimum between SRs of 0.6 and 0.8
- ➔ Residence time required under fuel-rich conditions is ~1 sec
- ➔ Fuel effects are minimal for cyclone firing

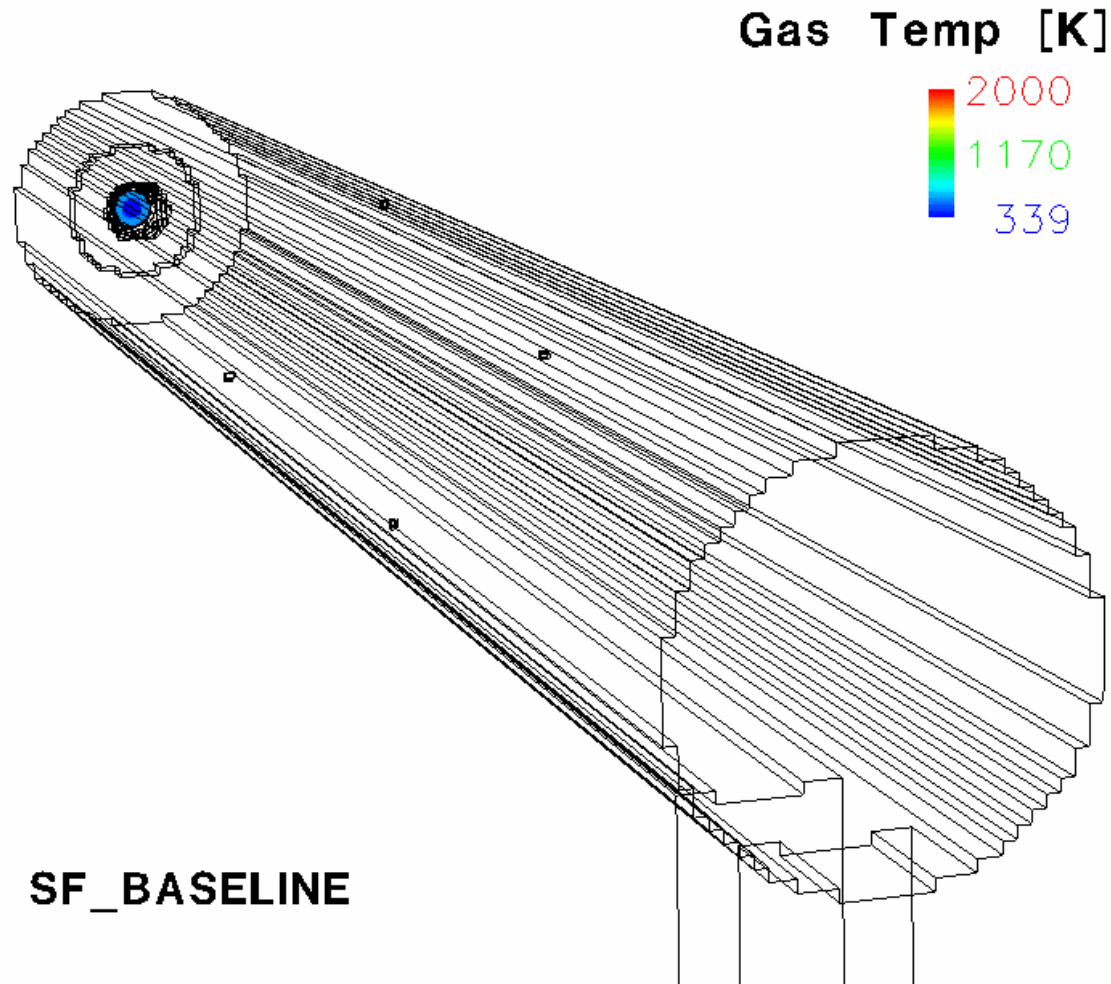


# Wood Co-firing



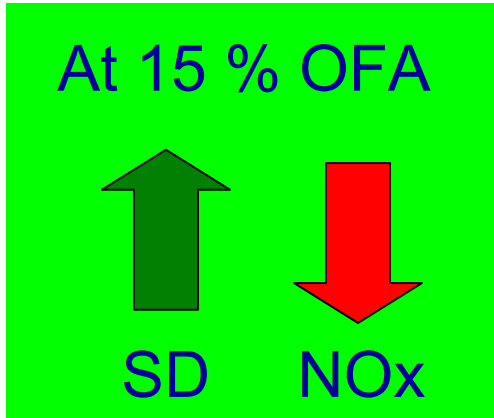
- ◆ **Pilot scale**
- ◆ **Two injection strategies**
  - » **co-milled**
  - » **separate center injection**
- ◆ **Simulations exhibit excellent agreement with detailed temperature measurements**
- ◆ **Post-processor for simulation of NO<sub>x</sub> chemistry**

# Temperature Predictions

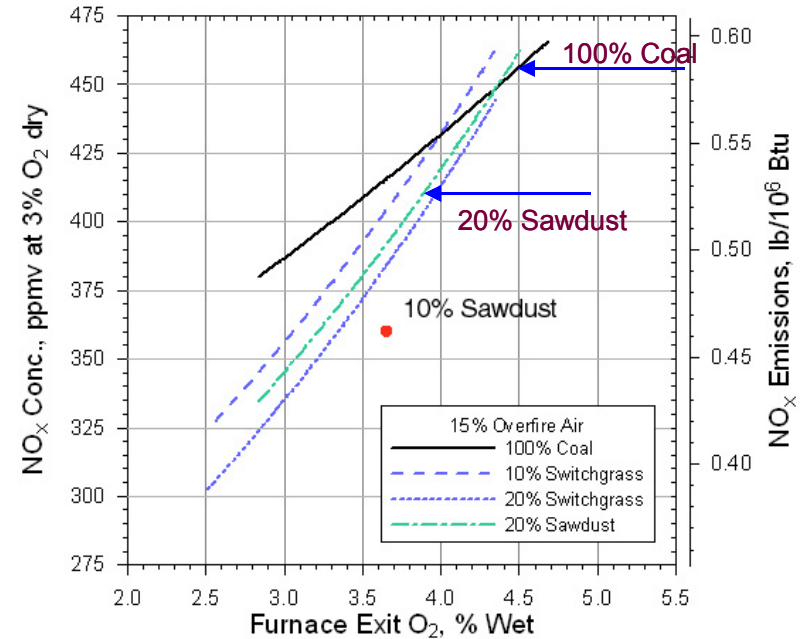
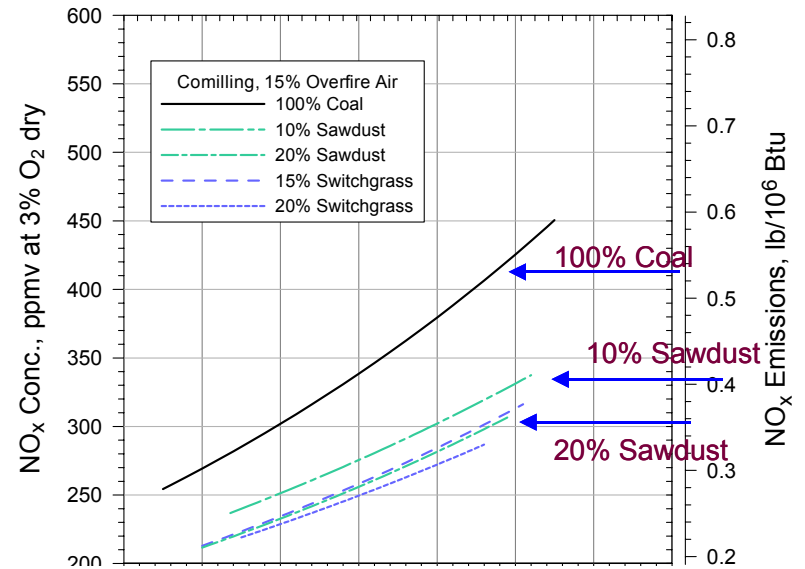
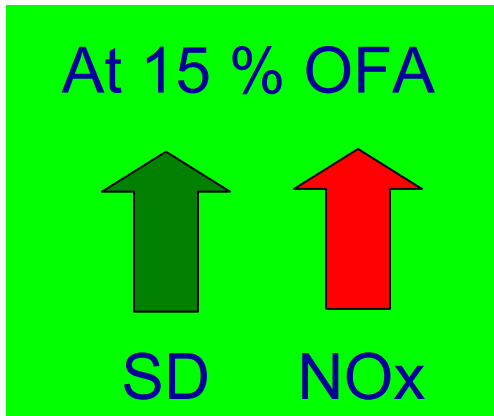


# NO<sub>x</sub> Measurements during Testing

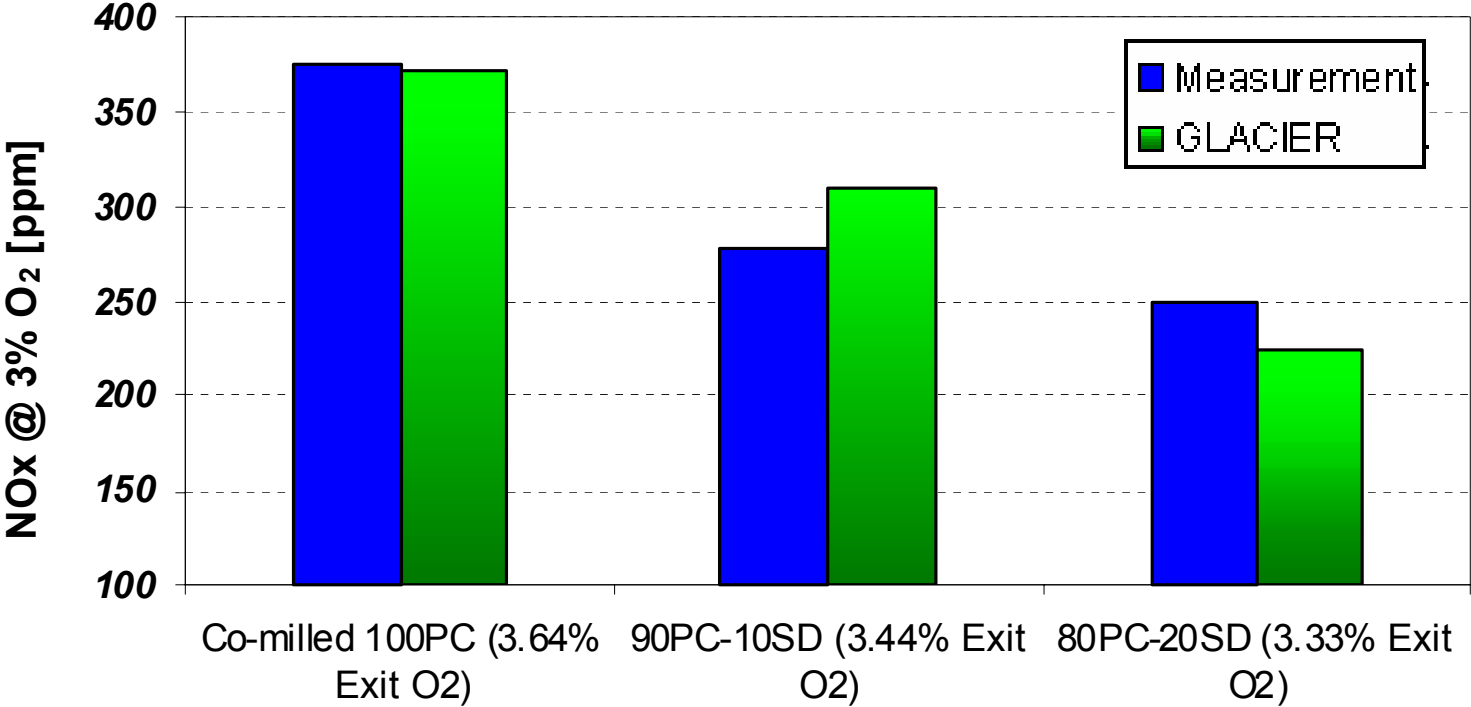
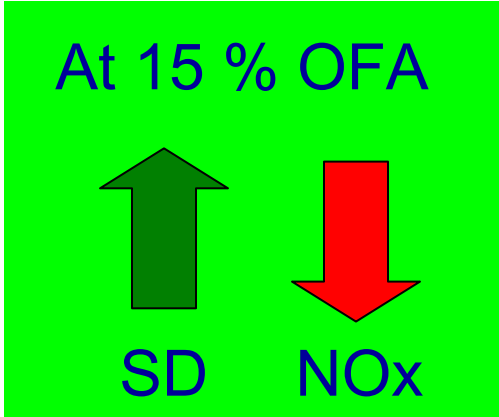
Co-milled



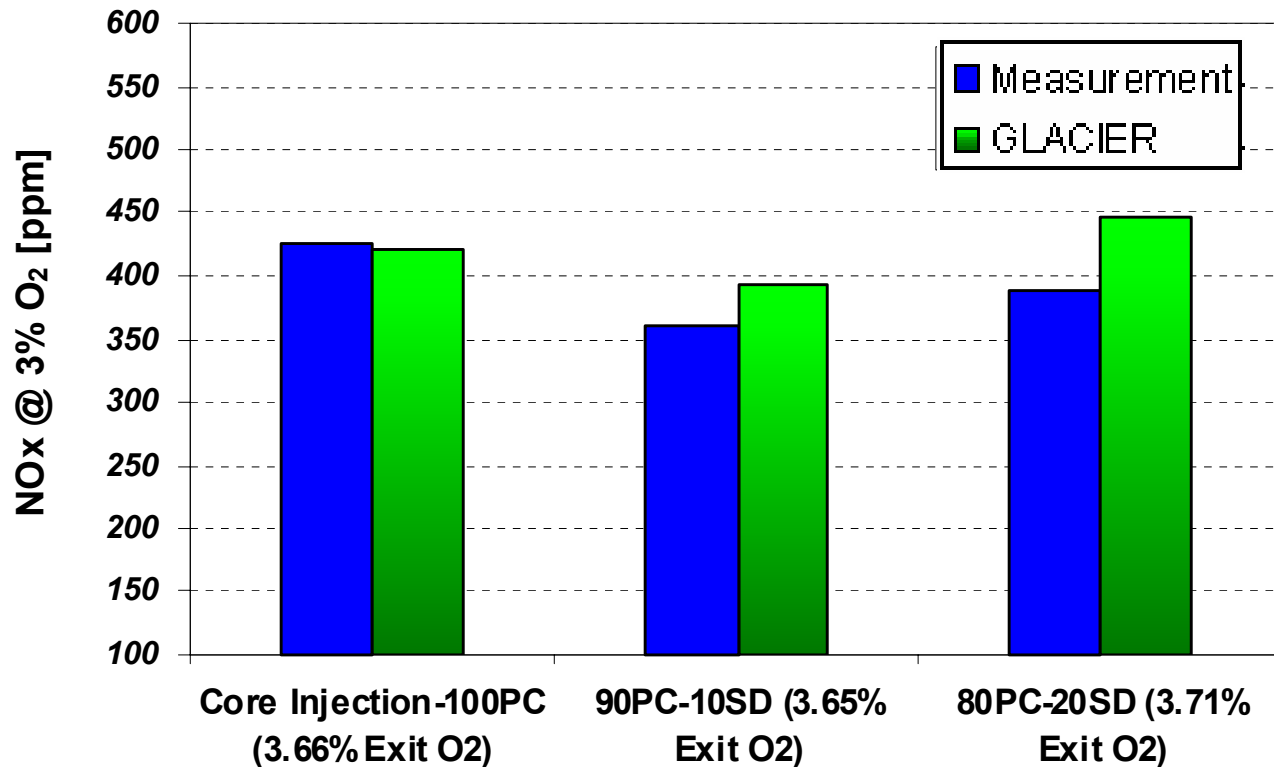
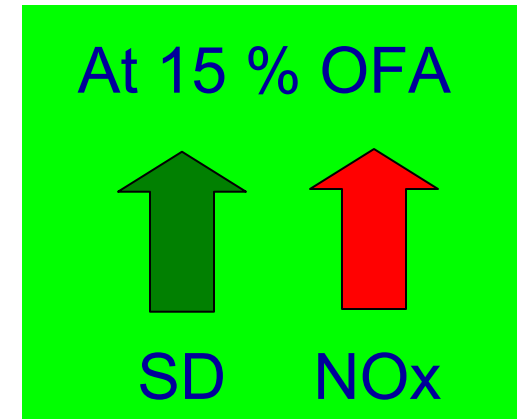
Center Injection



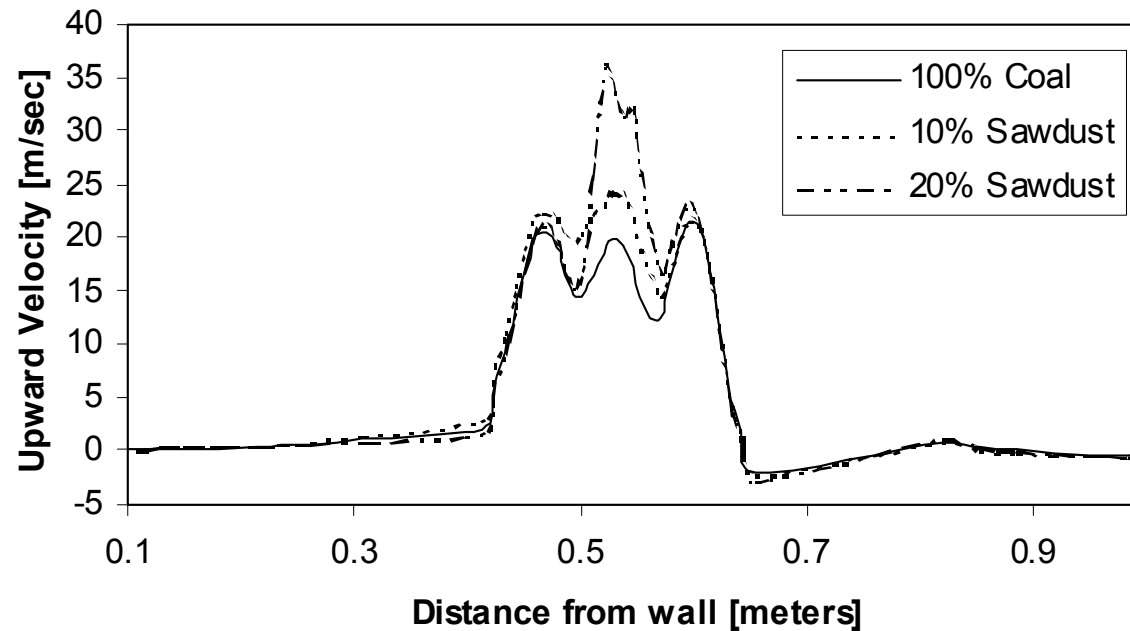
# Exit NOx Concentration: Co-milled



# Exit NOx Concentration: Center Injection



# Near Burner Velocity Profile



# Complex Nature of Fuel Effects on NO<sub>x</sub>

## → Two biomass injection scenarios

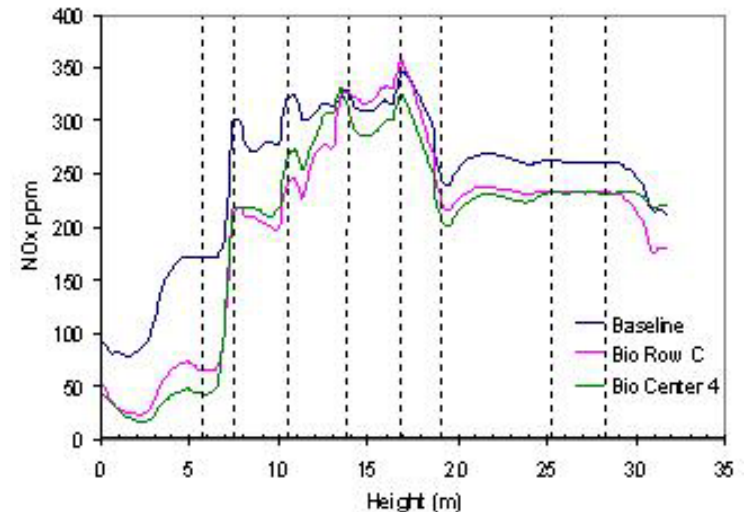
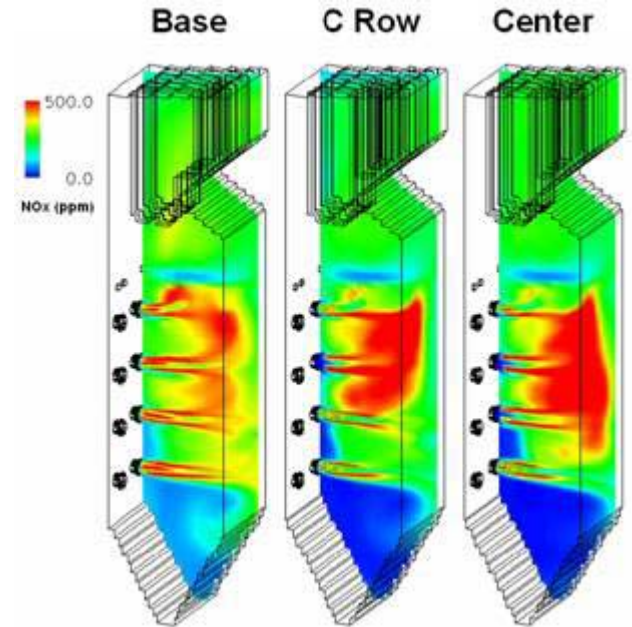
- ◆ Configuration 1: Four “C Row”
- ◆ Configuration 2: Center four burners
- ◆ 10% NO<sub>x</sub> reduction for both configurations
- ◆ Fuel nitrogen reduction accounts about half of total reduction

## → Volatility effect

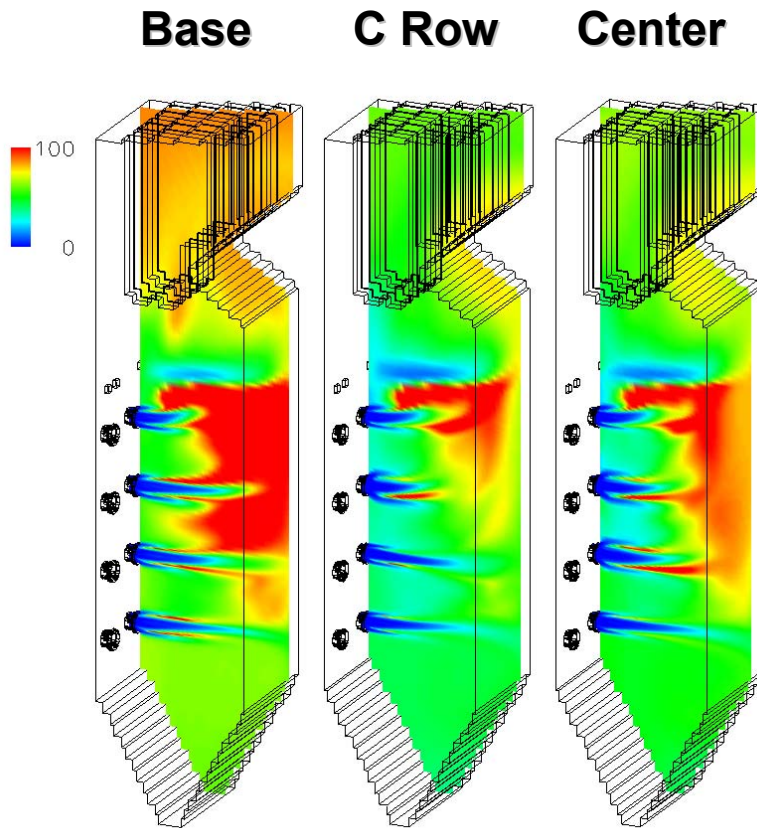
- ◆ Greater for center injection
- ◆ Wet biomass releases volatiles in lower furnace more effectively

## → Heating value effects

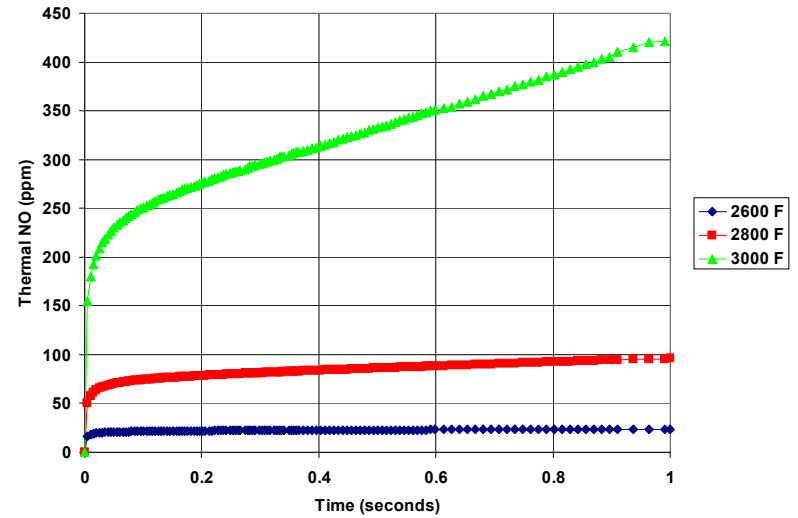
- ◆ Thermal NO<sub>x</sub> decrease greater for “C Row”
- ◆ Delayed mixing of volatiles leads to lower peak flame temperatures and extended NO reduction



# Thermal NOx



Thermal NOx (ppm)



# Coal Combustion Additives for NO<sub>x</sub> Control

Ohtsuka et al., Energy&Fuels (1998)

coal	Catalyst Loading (wt%)	Conversion of coal-N (%)						
		N <sub>2</sub>	NH <sub>3</sub>	HCN	Oil-N	Tar-N	Char-N	Total
LY	0.0	3.9	16.0	5.8	22.0	7.6	52.0	107
LY	0.7	49.0	10.0	2.1	10.0	5.4	25.0	102
LY	2.8	53.0	13.0	1.3	14.0	3.6	17.0	102
BA	0.0	7.8	17.2	4.7	12.5	3.1	62.5	108
BA	1.9	28.1	12.5	1.6	10.9	3.4	46.9	103

- Typically metallic, often nanoscale
- Application/dispersion challenges
- Related objectives in modifying fuel properties:
  - ◆ Enhance volatile yield
  - ◆ Enhance nitrogen yield during pyrolysis
- Potential co-benefits for combustion performance, slagging, corrosion, other emissions

# Reburning

## → Conventional Reburn

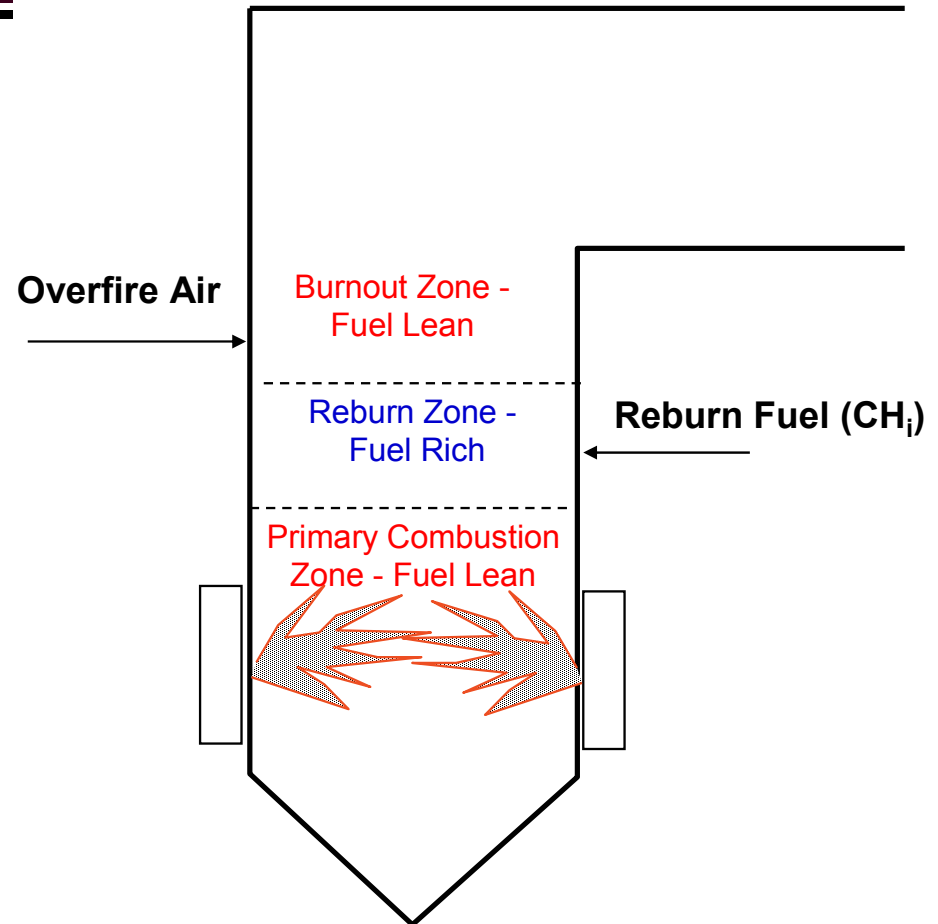
- ◆ >10% of thermal input
- ◆ OFA required
- ◆ Gas, coal, biomass

## → Fuel Lean Gas Reburn

- ◆ 5-7% of thermal input
- ◆ OFA not required
- ◆ Limited by CO emissions

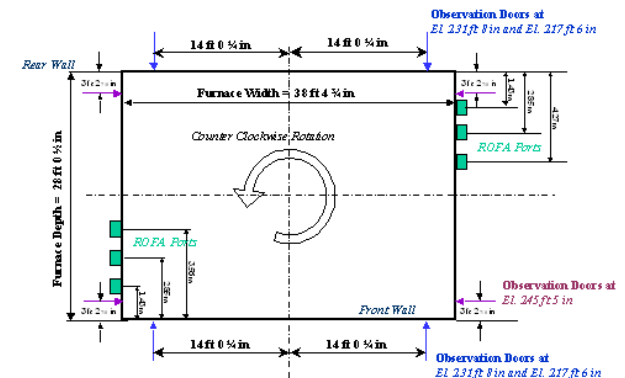
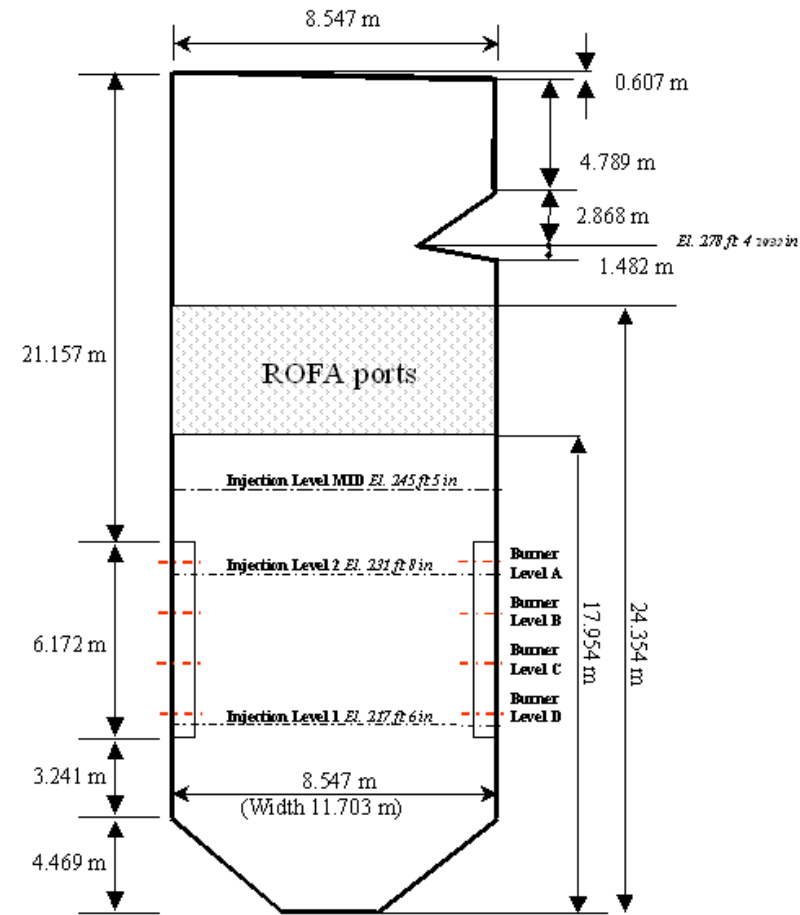
## → Amine enhanced fuel lean gas reburn

- ◆ Urea co-injected with gas
- ◆ Usually combined with FLGR and SNCR

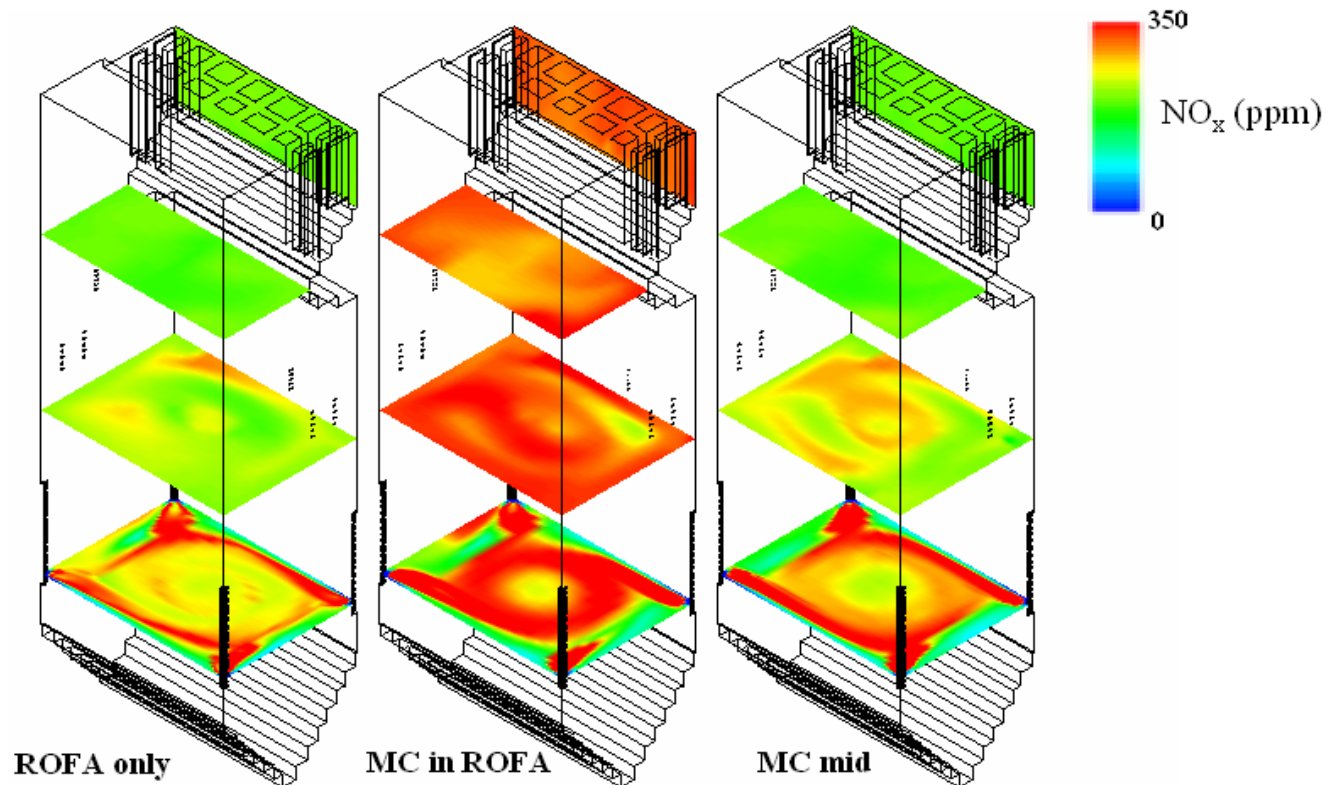


# Micronized Coal Reburn/Co-firing

- ➔ Micronized coal (~85%<325 mesh) vs. pulverized coal (~75%<200 mesh)
- ➔ DOE Demonstration on a staged 143 MW T-fired unit
- ➔ 16% pulverized coal replacement
- ➔ MC injection evaluated at multiple locations/elevations including:
  - ◆ conventional reburn location between burner stack and OFA with OFA
  - ◆ upper and lower burner stack elevations

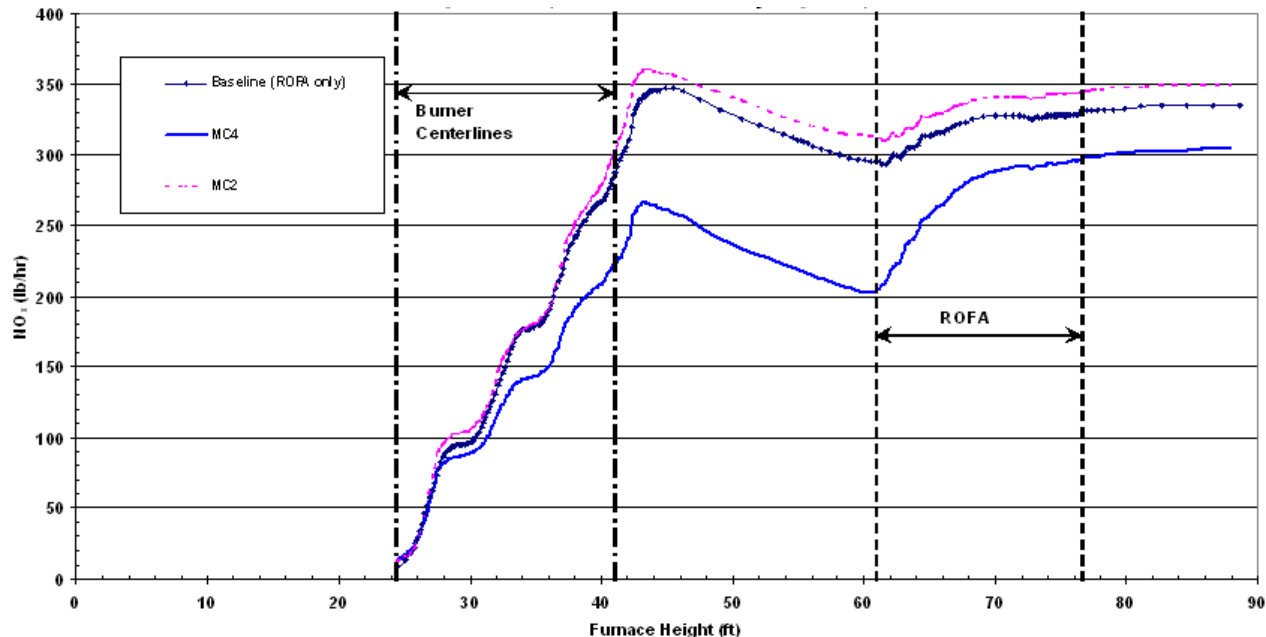
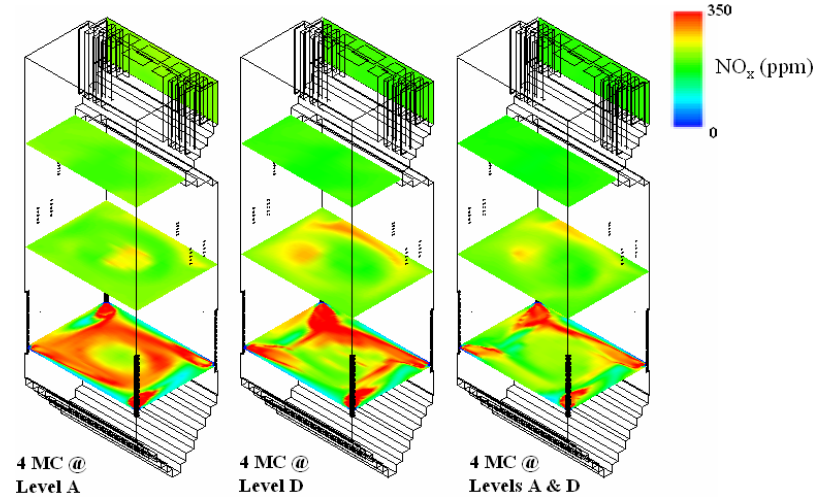


# Micronized Coal "Reburn" Results

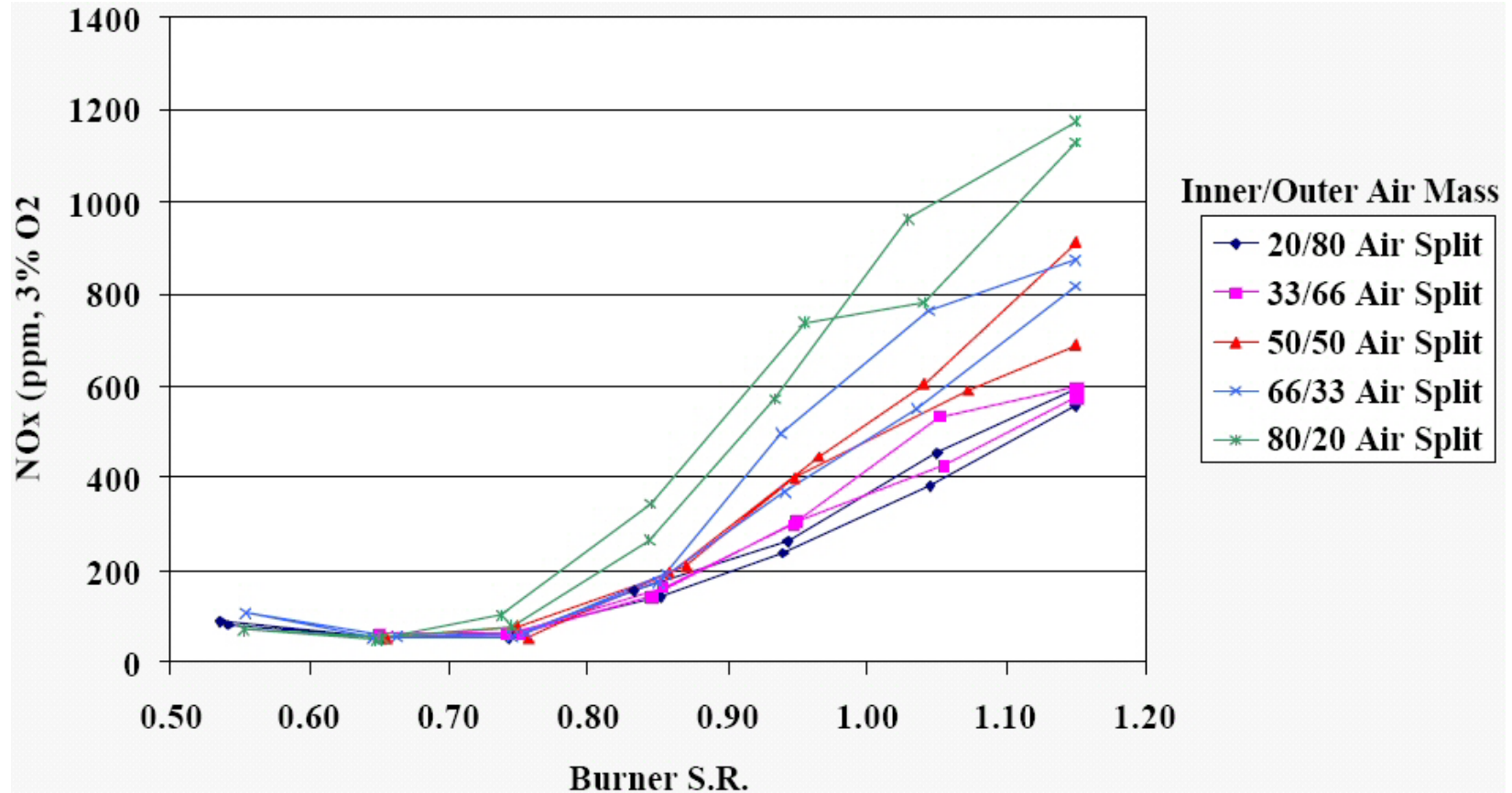


# Micronized Coal "Co-firing" Results

- Micronized coal enhances lower furnace volatile yield
- Co-firing more effective than reburn
- Creating uniformly rich conditions across furnace cross section most effective



# Deep Staging



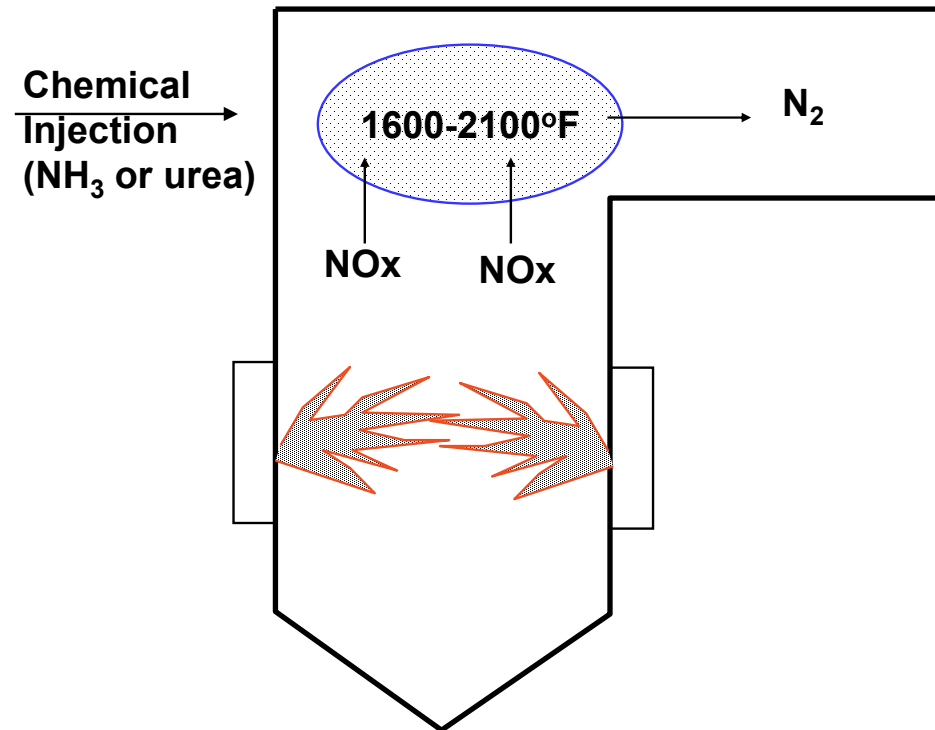
# Selective Noncatalytic Reduction (SNCR)

## → Benefits:

- ◆ Low cost compared to SCR
- ◆ Significant NO<sub>x</sub> reductions (>50%) in small units
- ◆ 25-30% reduction with <5 ppm NH<sub>3</sub> slip recently demonstrated in 600 MW unit

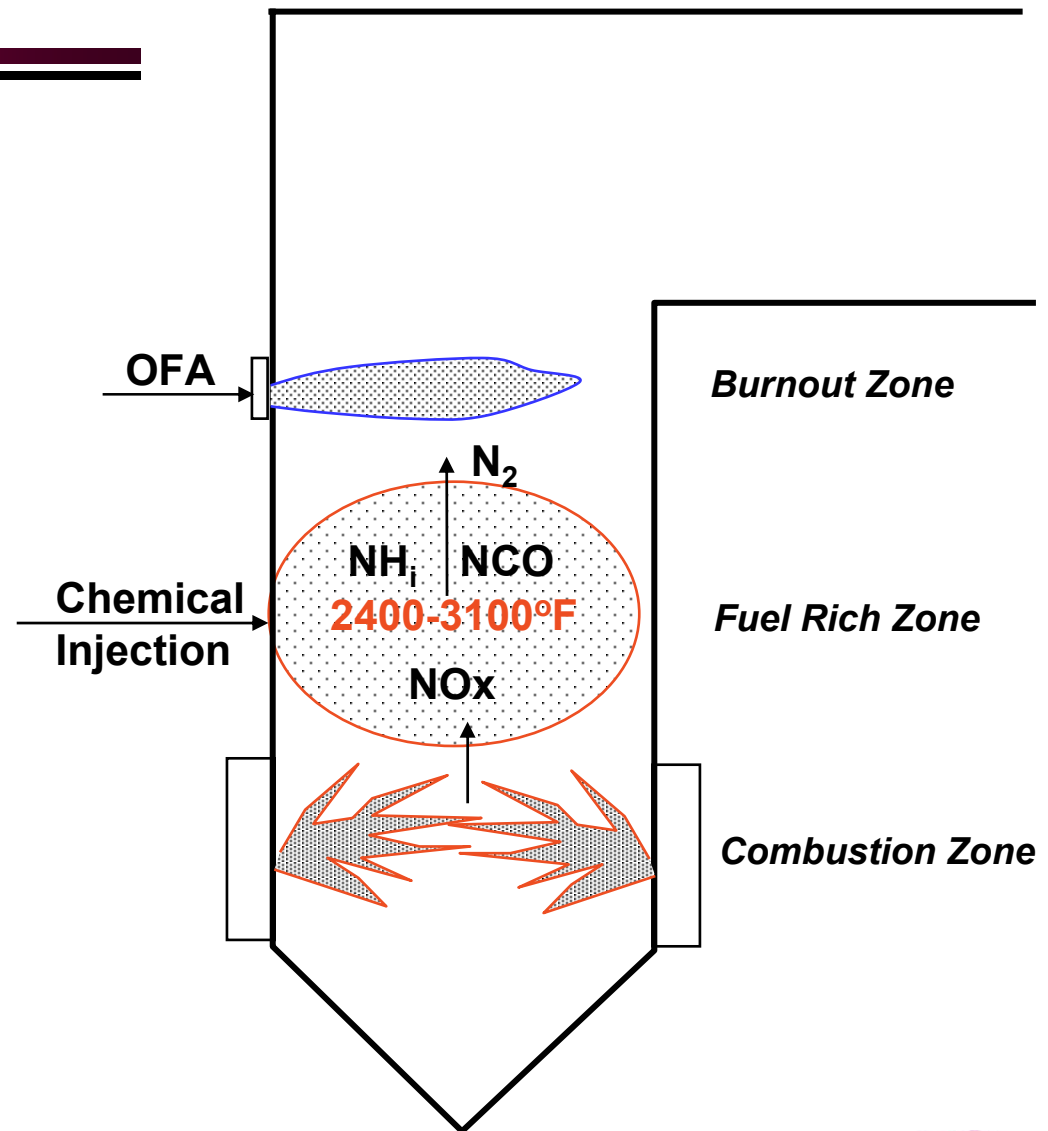
## → Difficulties:

- ◆ Mixing limitations
- ◆ Temperature window may not be accessible
- ◆ Other emissions may increase (NH<sub>3</sub> and N<sub>2</sub>O)

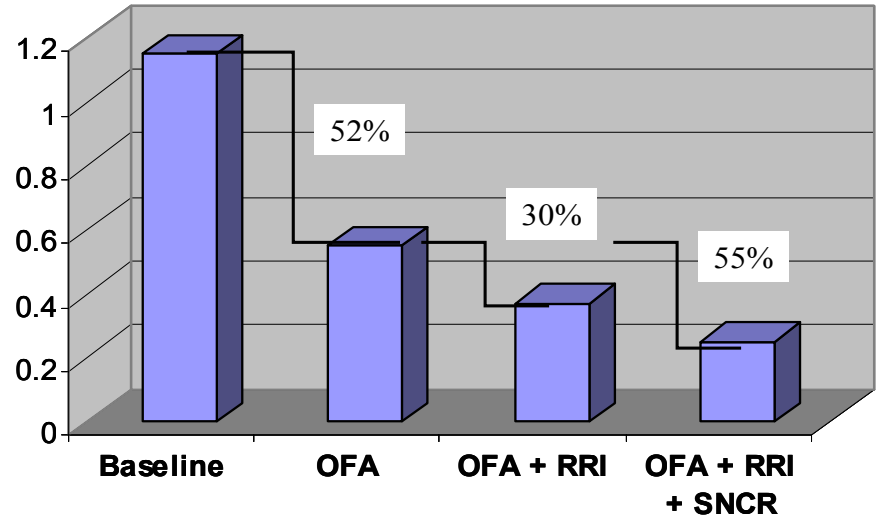


# Rich Reagent Injection

- Significant NO<sub>x</sub> reductions achievable by air staging
- Staging creates a hot, fuel rich lower furnace
  - ◆ In-situ reburning
  - ◆ NO<sub>x</sub> reduction improves with reduced SR and increased res. time
- Amine reagents accelerate the rate of NO<sub>x</sub> reduction
  - ◆ NO<sub>x</sub> reduction in rich zones
  - ◆ NO<sub>x</sub> formation in lean zones

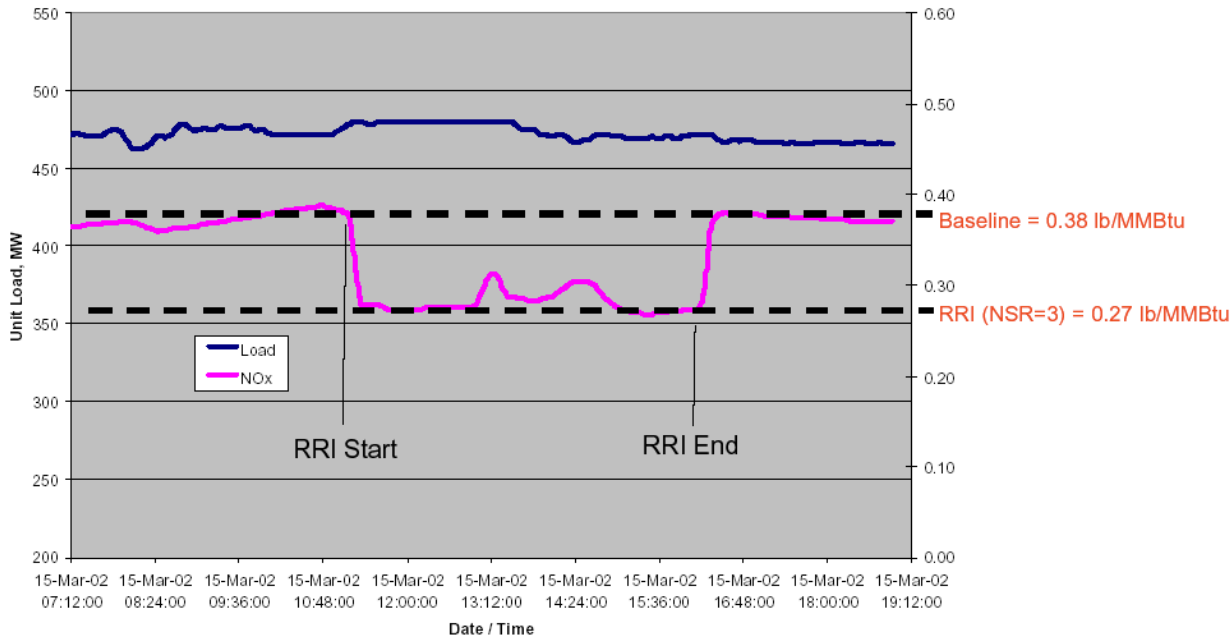


# RRI Field Results



Conective BL England Station

## Ameren Sioux Station

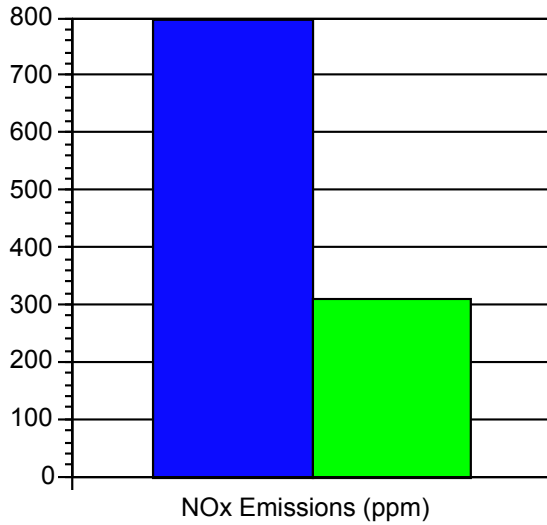


# Balance of Plant

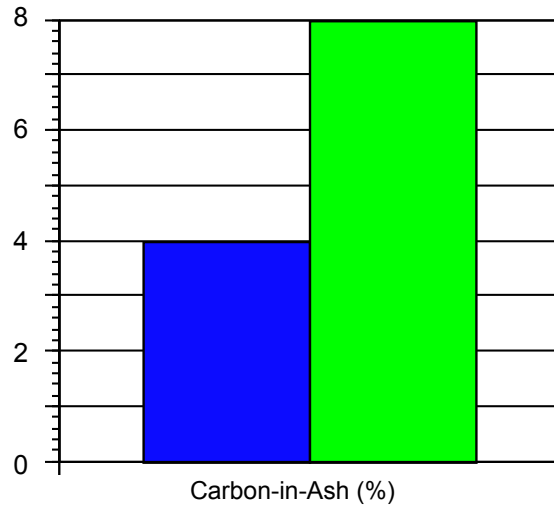
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- **Carbon Monoxide Emissions**
- **Carbon-in-Flyash (LOI)**
- **Waterwall Corrosion**
- **Heat balance and Efficiency**
- **Combustion Equipment Complexity and Performance**
  - ◆ **Coal pipe fires**
  - ◆ **Burner/air port maintenance**
  - ◆ **FD fan requirements**
  - ◆ **Fine particle emissions (ash & soot)**

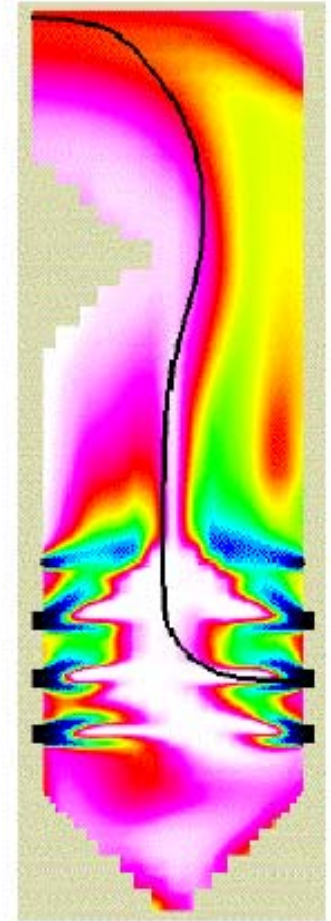
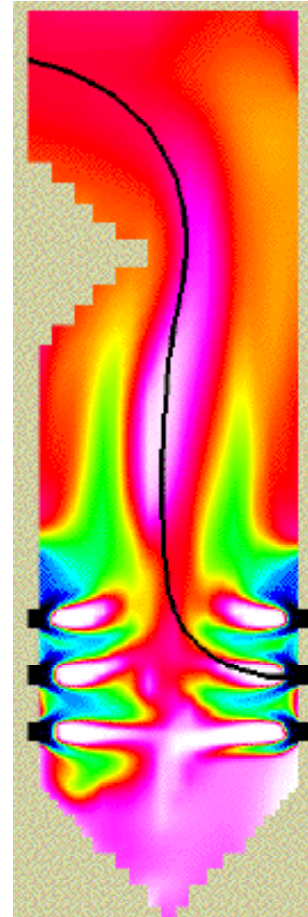
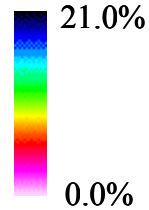
# Carbon in Flyash



■ Post Retrofit  
■ Pre Retrofit

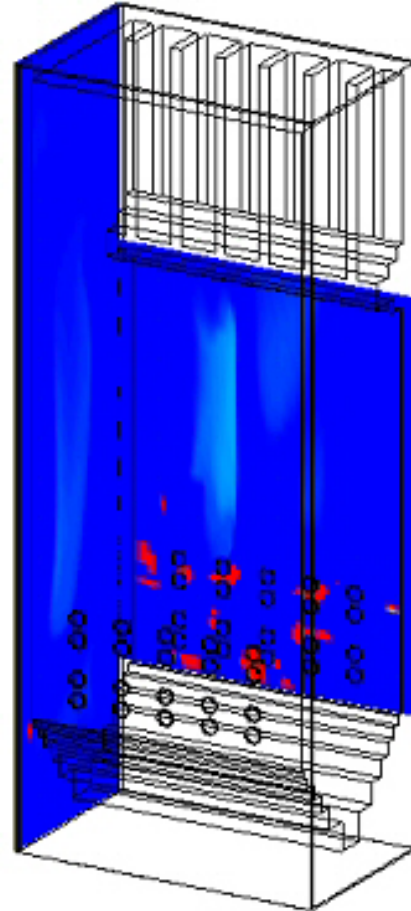


O<sub>2</sub> Concentration

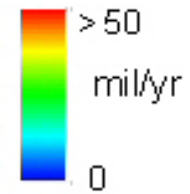
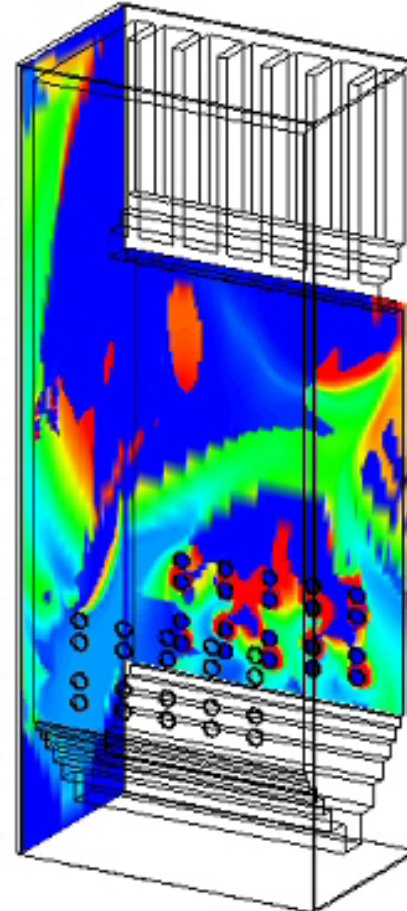


# Corrosion and Staging

SR = 1.2



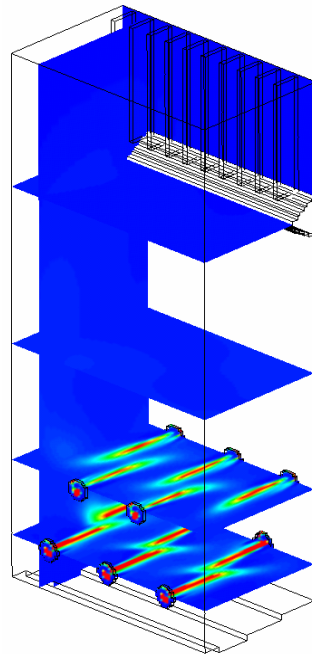
SR = 0.8



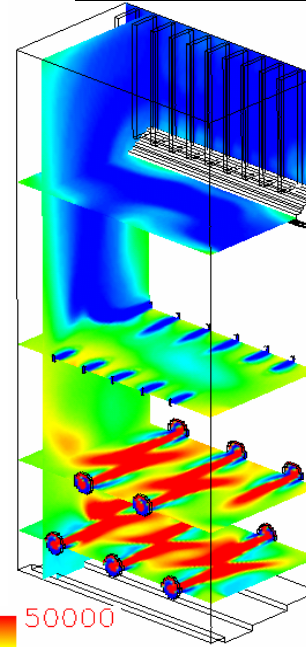
# Carbon Monoxide Levels

- Emissions
- Efficiency
- Safety
- Black Bottom (soot)

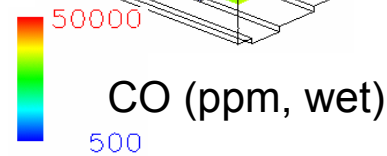
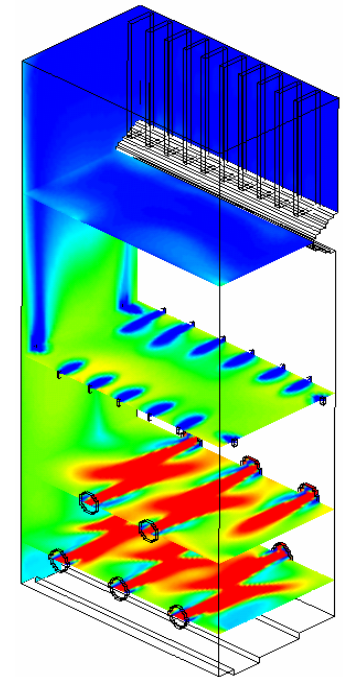
Baseline



OFA Case 1



OFA Case 2

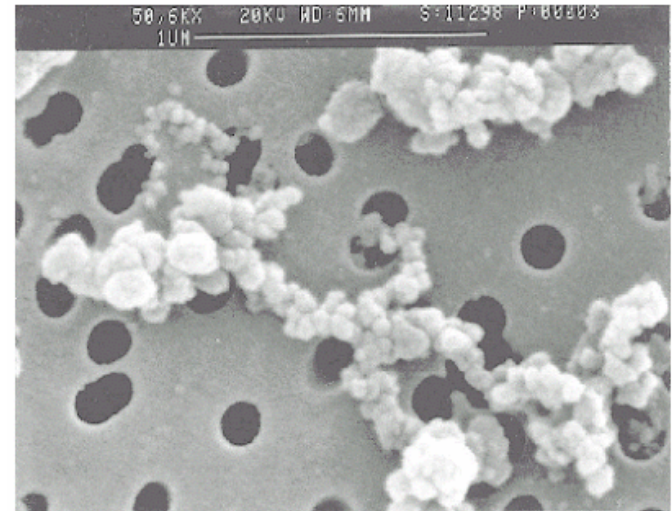
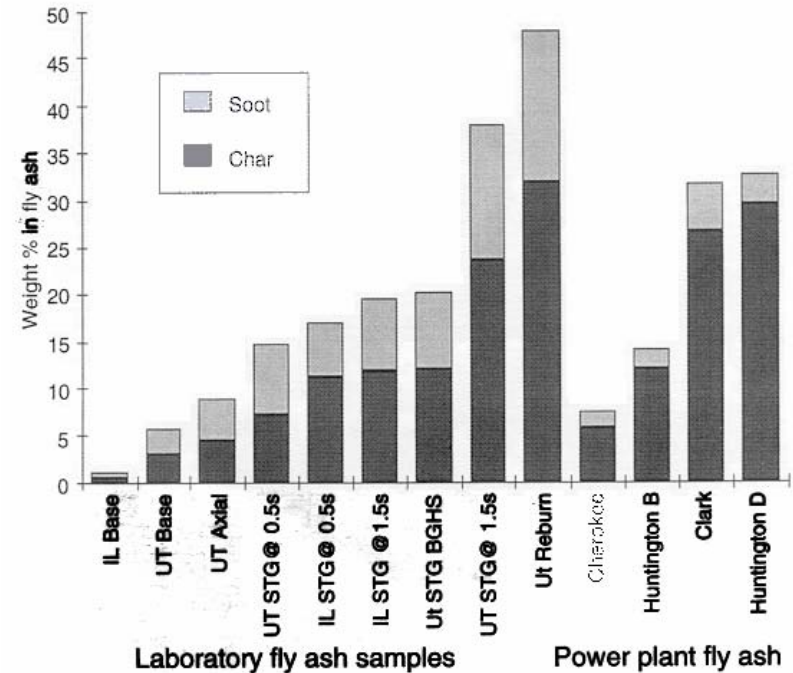


# Soot in Low NOx Flames

→ Low-NOx combustion can result in significant concentrations of submicron soot particles

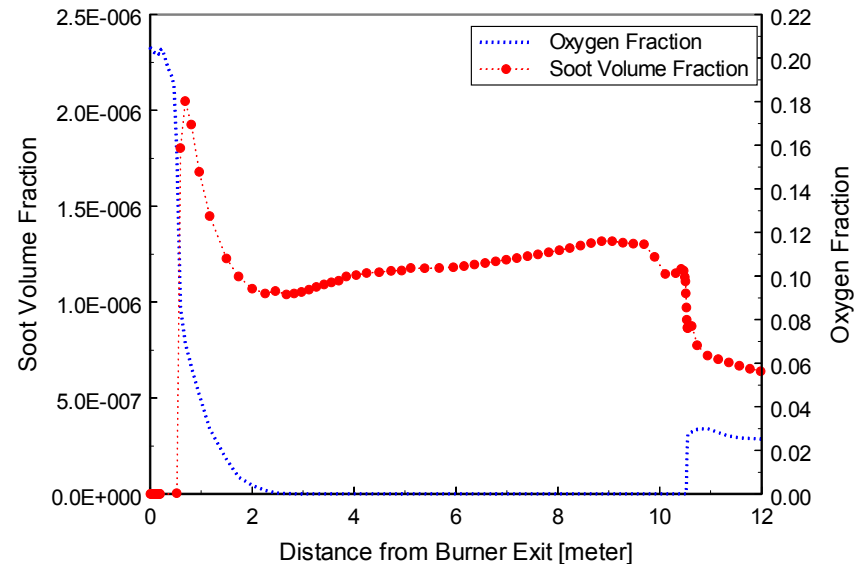
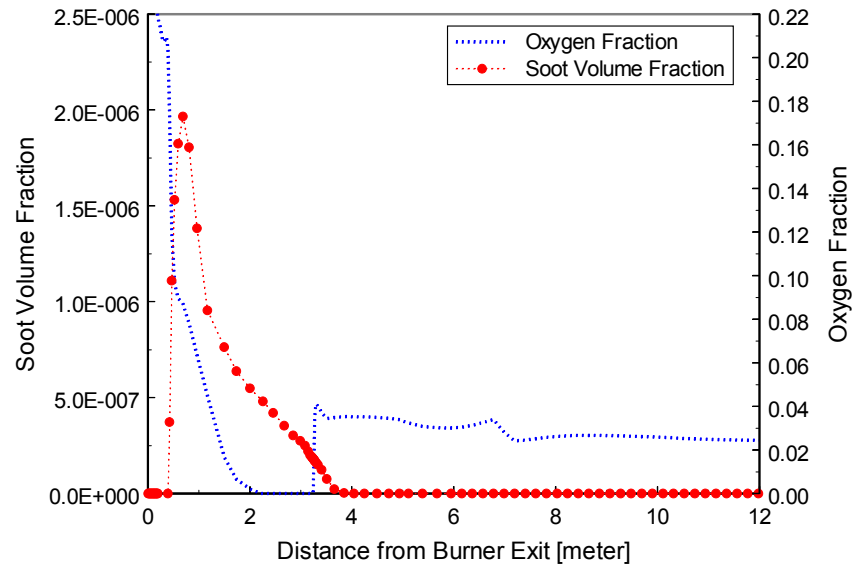
→ Potential Impacts:

- ◆ Increase in fine particulate emissions and opacity
- ◆ Boiler heat imbalances due to enhanced lower furnace radiation
- ◆ Potential decrease in effectiveness of air staging for NOx control
- ◆ Potential impact on high temperature reagent injection effectiveness
- ◆ Ash salability



# Pilot-scale Modeling Insight

- ➔ Reasonable soot concentrations are predicted
- ➔ A residence time threshold exists for soot breakthrough under typical low-NO<sub>x</sub> conditions



# Summary

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- ➔ **Target fuel and the importance of fuel flexibility play a key role in NOx control technology selection**
- ➔ **Appropriate fuel selection can enable attainment of substantially lower NOx emissions**
- ➔ **Balance of plant impacts must be considered when NOx control technology & fuel selection decisions are made**